

# Capture Process Selection and Cost Analysis

for

## The First CCS Pilot Project in China

*Professor: Pi Jinlin*

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2010-11-4



# *WUHUAN'S Engineering Office*



**五环科技股份有限公司**

**Wuhuan Engineering Co., Ltd**

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# Brief Introduction to Wuhuan Engineering Co.,LTD

- ◇ An national grade design institute with the history of over 50 years; Rank within top 20 engineering firms many times in China .
- ◇ Focus engineering fields: Coal chemical, ammonia, NH<sub>3</sub> processing, phosphate chemical and synthetic materials industries. Over 50% of NH<sub>3</sub>, Ur and methanol capacity in China were constructed from Wuhuan's engineering.
- ◇ Many significant domestic chemical projects were designed by Wuhuan.
- ◇ The annually contract price : RMB 8 billion ( EPC and engineering service).
- ◇ Professionals (engineers and experts): 1200, including 2 National Design Masters and 37 experts with national subsidy.
- ◇ Address: 1019 Minzu Road, Wuhan, P.R. China
- ◇ Website: CWCEC.COM



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## *Wuhuan\_ Reference of the built large and middle-sized projects (over1000)*

<i>Ammonia、Methanol、Coal Chemical、Natural Gas Chemical</i>	<i>252</i>
<i>Chemical Fertilizer</i>	<i>233</i>
<i>Nitric Acid、Sulfuric Acid、hydrochloric acid</i>	<i>38</i>
<i>Caustic soda、Soda ash</i>	<i>14</i>
<i>Inorganic salts chemical ,</i>	
<i>Fine Chemical, Food, Pharmaceutical, Chemical pesticides</i>	<i>41</i>
<i>Petrochemical、Organic chemical</i>	<i>30</i>
<i>Town gas、LPG and Oils storage engineering</i>	<i>61</i>



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*Wuhuan \_ Reference of the built large-sized and middle-sized projects (To be continued)*

<i>Thermal power engineering</i>	<i>45</i>
<i>ASU</i>	<i>19</i>
<i>Composite material</i>	<i>11</i>
<i>Environmental protection and impact</i>	<i>86</i>
<i>City planning and civil architecture</i>	<i>152</i>
<i>Project cost estimate</i>	<i>320</i>
<i>Project supervision</i>	<i>53</i>
<i>Project EPC contracting</i>	<i>46</i>



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## Wuhuan \_\_ Awards and Patents

■ <b>Awards</b>	<b>212</b>
<b>Thereinto: National</b>	<b>40</b>
<b>Provincial</b>	<b>156</b>
■ <b>Patents</b>	<b>28</b>



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Welcome Cooperation! Thanks!

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# Content

- **Project Overview**
- **Configuration of Units**
- **Capture Process Selection / Eng. Schemes**
- **Investment estimate and Cost Analysis**
- **Conclusion**



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# 1.Project Overview\_Background

Project Owner: Shenhua Group

Project objectives:

- to construct and operate the first pilot CCS project in China,
- to gain the knowledge and experience of capture, transportation and CO2 storage in aquifers .
- to provide experience and data support as requested for the construction and operation of commercial CCS project with injection capacity of over million tons /a

Injection Capacity : 10kt/a

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# 1.Project Overview\_Background

CO2 Source: Vent gas of Acid Gas Removal Unit of Coal to Hydrogen Plant in CTL Complex  
with CO2 concentration of 87%

Overall Process: Compression, Purification, Separation, Liquefaction, Transportation, Injection

Project Site: Yijinhualuoqi , Ordos, in Inner Mongolia, Ordos basin.

--Capture and Liquefaction Units: inside Shenhua CTL

-- Injection and Storage Reservoir : 20km from the Complex

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# 1.Project Overview\_Schedule

- July, 2009,  
Shenhua Group entrusted Wuhuan Engineering responsible for project feasibility study, basic engineering and detailed engineering .
- Up to now,  
Engineering completed,  
Installation and construction almost completed,  
Expected to inject CO2 into underground in December of 2010.



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# 1. Project Overview

## \_ Technical and Economical Index

No.	Items	Unit	Amount	Remark
1	CCS capacity	kt/a	10	
2	operation time	Hours/a	7440	
3	CO2 Specification			
	Food grade CO <sub>2</sub>	kt/a	10	After completion of the pilot operation
4	Consumption			
4.1	Feed CO <sub>2</sub>	k t/a	13.7	
4.2	Power	kWh/h	2322	
4.3	Cooling water	t/h	269	
4.4	LP Steam	t/h	0.5	
5	Capital Investment	M RMB	~2	
6	Cost of CCS	RMB/tCO <sub>2</sub>	277	41\$/t



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## 2.Configuration of Units\_Capacity

- Injection capacity:
  - 13.4 t/h (Food grade/Storage grade liquid CO<sub>2</sub>)
  - 322.6 t/d
  - 10 kt/a
- Operation system:
  - Annual operation days: 310 d/a
  - Daily operation hours: 24 h/d
  - Annual operation hours: 7440h/a



## 2. Configuration of Units \_ CO2 Product Specification

Product	Design requirements	Remark
Storage Liquid CO2	Purity $\geq 95\%$	
	Pressure: 1.7~2.2MPa.G	
Food grade CO2	Purity $\geq 99.9\%$	GB10621-2006



## 2. Configuration of Units \_ WBS

- Level 1:
  - Ground facilities (capture and transportation facilities)
  - Underground engineering and monitoring system (storage system)
- Level 2: Ground facilities:
  - CO2 Compression,
  - Purification,
  - Liquefaction and Distillation,
  - Refrigeration System,
  - Storage and Transportation,
  - Utility distribution
  - Control system



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## 2. Configuration of Units \_ WBS

- Level 2: Underground Engineering and Monitoring System:
  - Injection Well
  - Monitoring Well
  - Underground Storage Reservoir

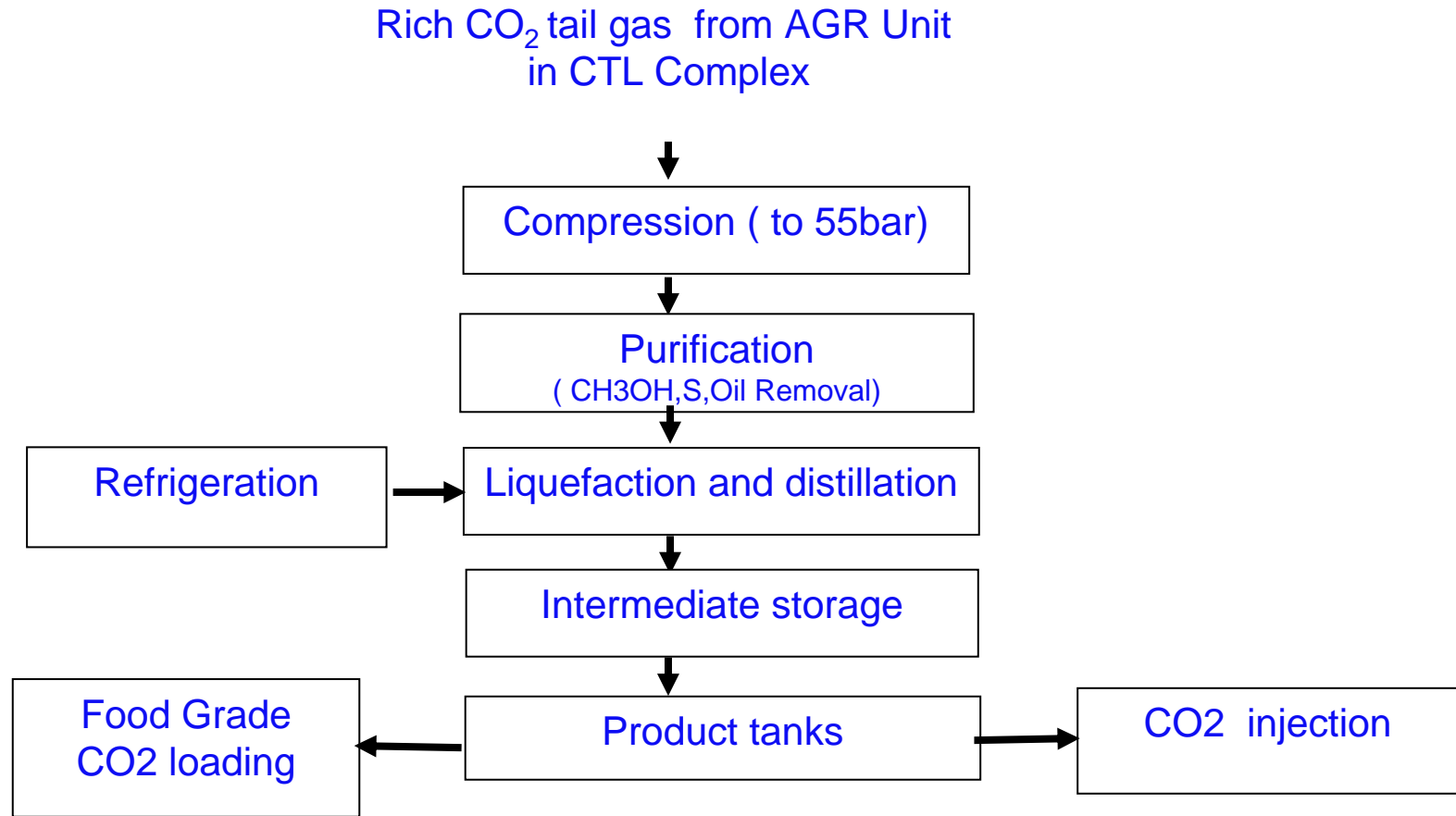


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## 2. Configuration of Units\_ Process Flow Block Diagram



### 3. Process Selection \_ CO2 Feed

	Design data, mol%	Actual data, mol%
T (°C)	25.5	25--30
P(MPag)	0.105	0.08—0.10
CO2	87.938	83--88
CO	0.0178	TRACE
H2	0.17	1.1—1.25
N2	10.503	11--15
H2O	1.358	TRACE
H2S	0.000341	TRACE
CH3OH	0.009955	5—12ppm
CH4	0.001156	0.01—0.02
Ar	0.001182	0.01—0.05



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### 3. Selection of Capture Process

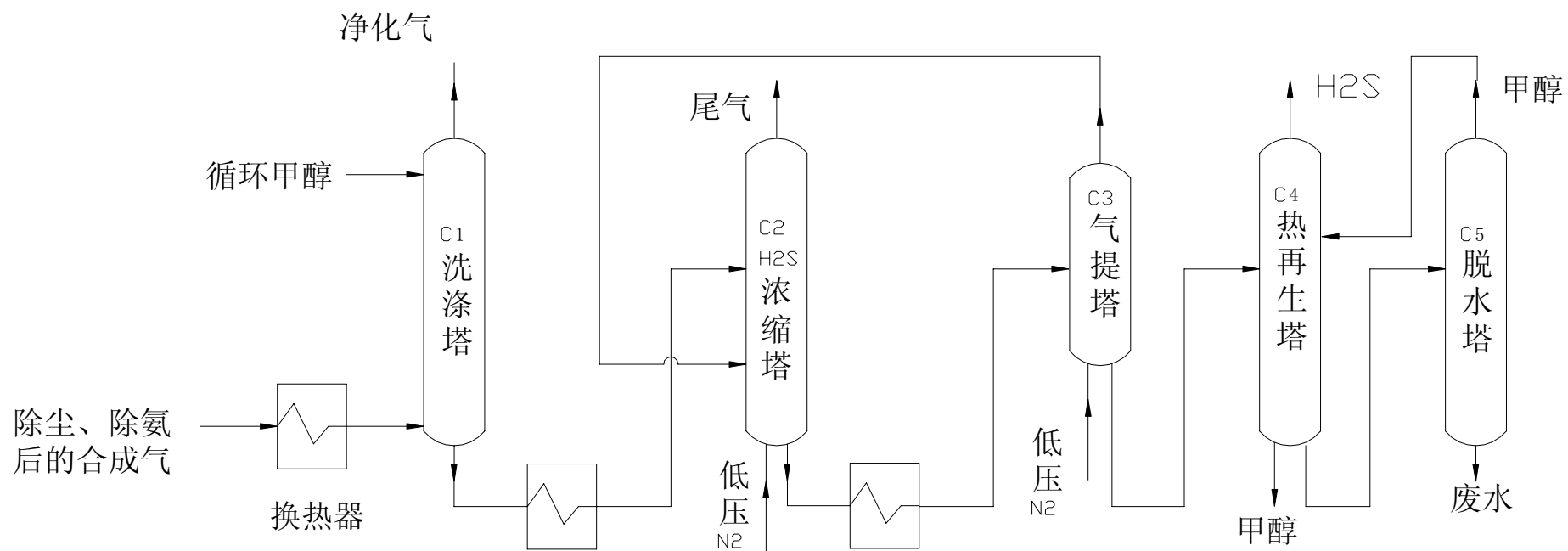
#### Option 1: Revamping of Rectisol Unit to rise up CO<sub>2</sub> concentration

Restore the existing flow into the typical Rectisol process of ammonia industry.

Main revamping including:

- add one CO<sub>2</sub> product column (new CO<sub>2</sub> column) ;
- add one set of spiral wound heat exchanger;
- add one set of LT heat exchanger and LT pump, etc.



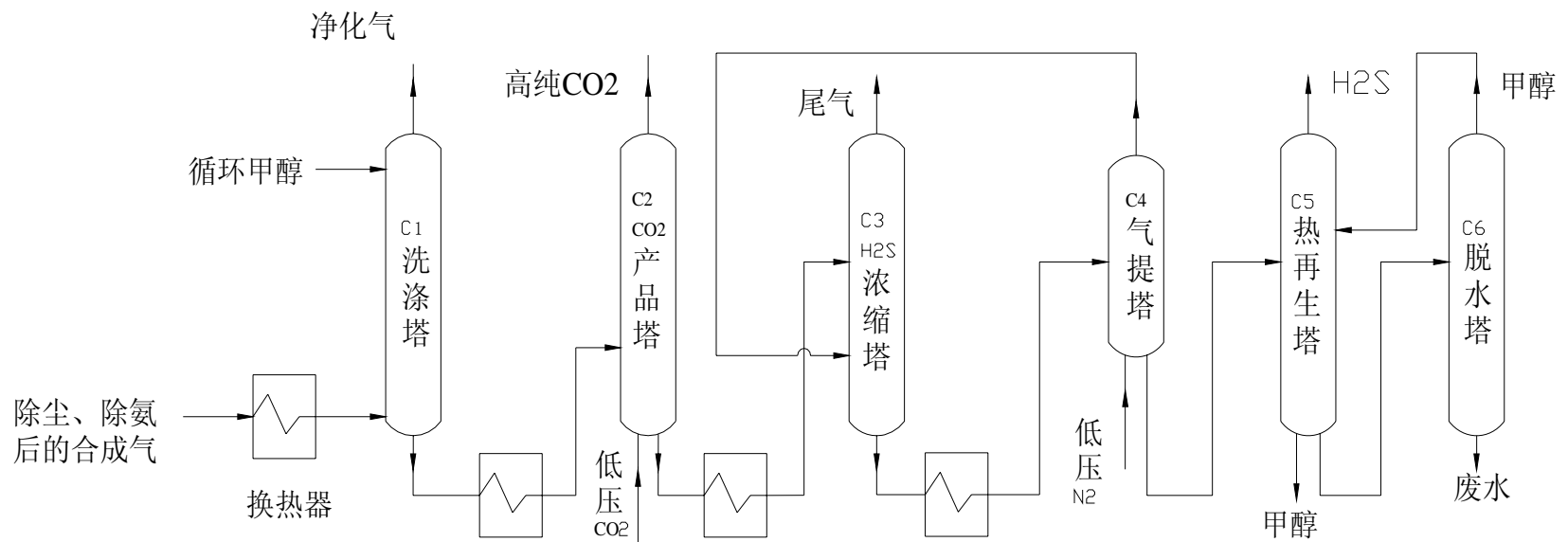


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### 3. Selection of Capture Process

#### Option 2: Installation of additional Purification and concentration System

An additional system which adopts TSA and LT distillation technology is installed for purification and concentration of CO<sub>2</sub> into liquefied phase.

A typical food grade CO<sub>2</sub> process will be employed



## \_Comparison of Options

Item	Option 1	Option 2
CO <sub>2</sub> Sequestration Spec.	Satisfied	Satisfied
Food Grade CO <sub>2</sub> Spec.	No	Yes
Construction period	> 12 months	~10 months
Impact on CTL operation	CTL Complex shutdown for > 12 months	No impact on CTL operation
Layout limit	Limited, no space for additional equipments	Available, to be installed on spare area of CTL Complex.

Option 2 is picked up.



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# \_Pressure Selection of Purification and Liquefaction

Utilities Consumption at Different Liquefied Pressure (On tons of CO<sub>2</sub>)

Consumption	Pressure of purification and liquefaction (MPa)			
	2.5	4	5	7.8
Cooling water ( $\Delta t=12^{\circ}\text{C}$ ) m <sup>3</sup>	28.9	22.4	18.8	19.2
Raw gas compression power (kW)	215.9	106.1	107.3	118
NH <sub>3</sub> compression power (kW)	60.7	62	49.4	42.6
Total power consumption (kW)	276.6	168.1	156.7	160.6

5.0MPa is chosen for purification and liquefaction.

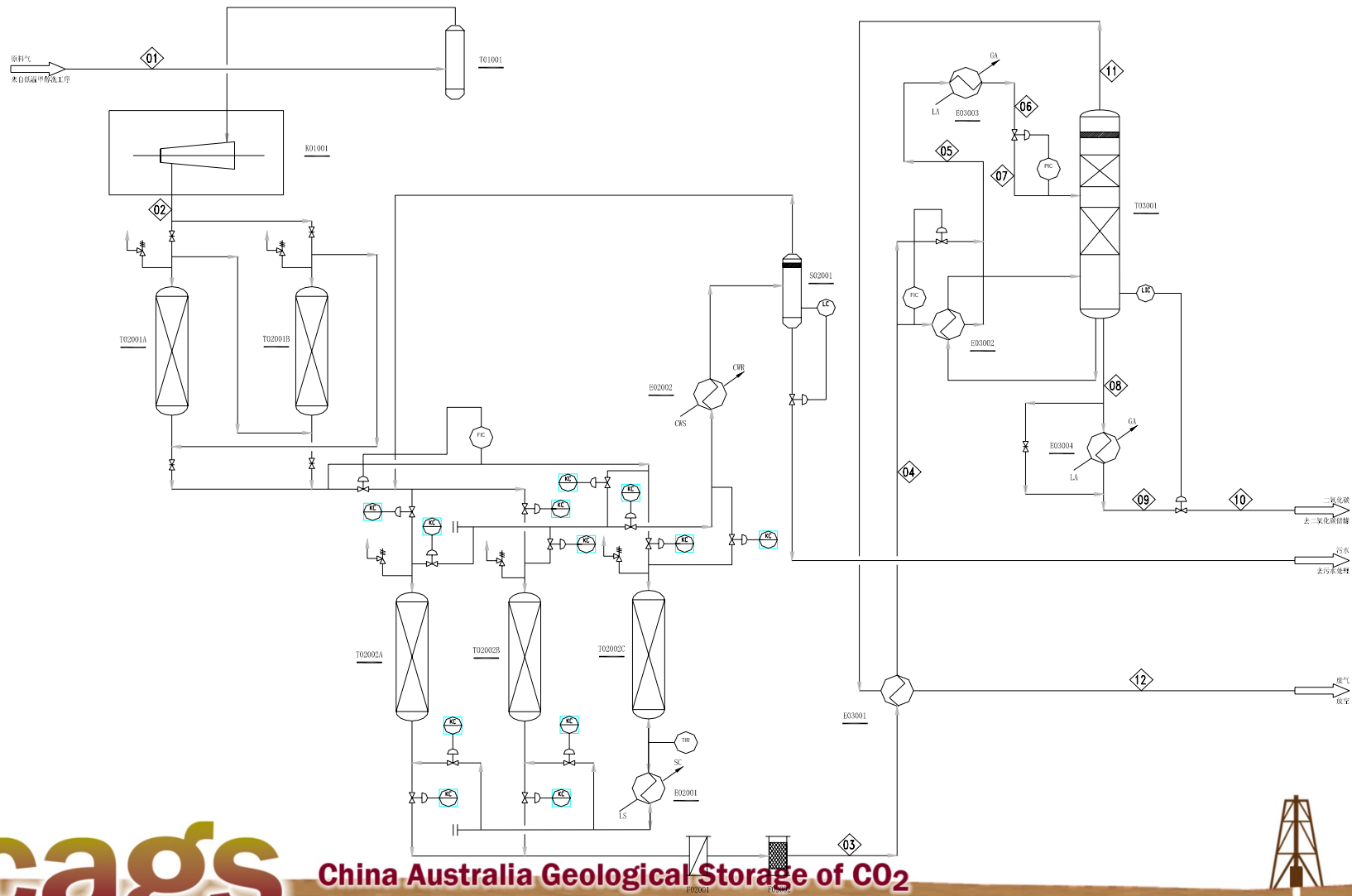


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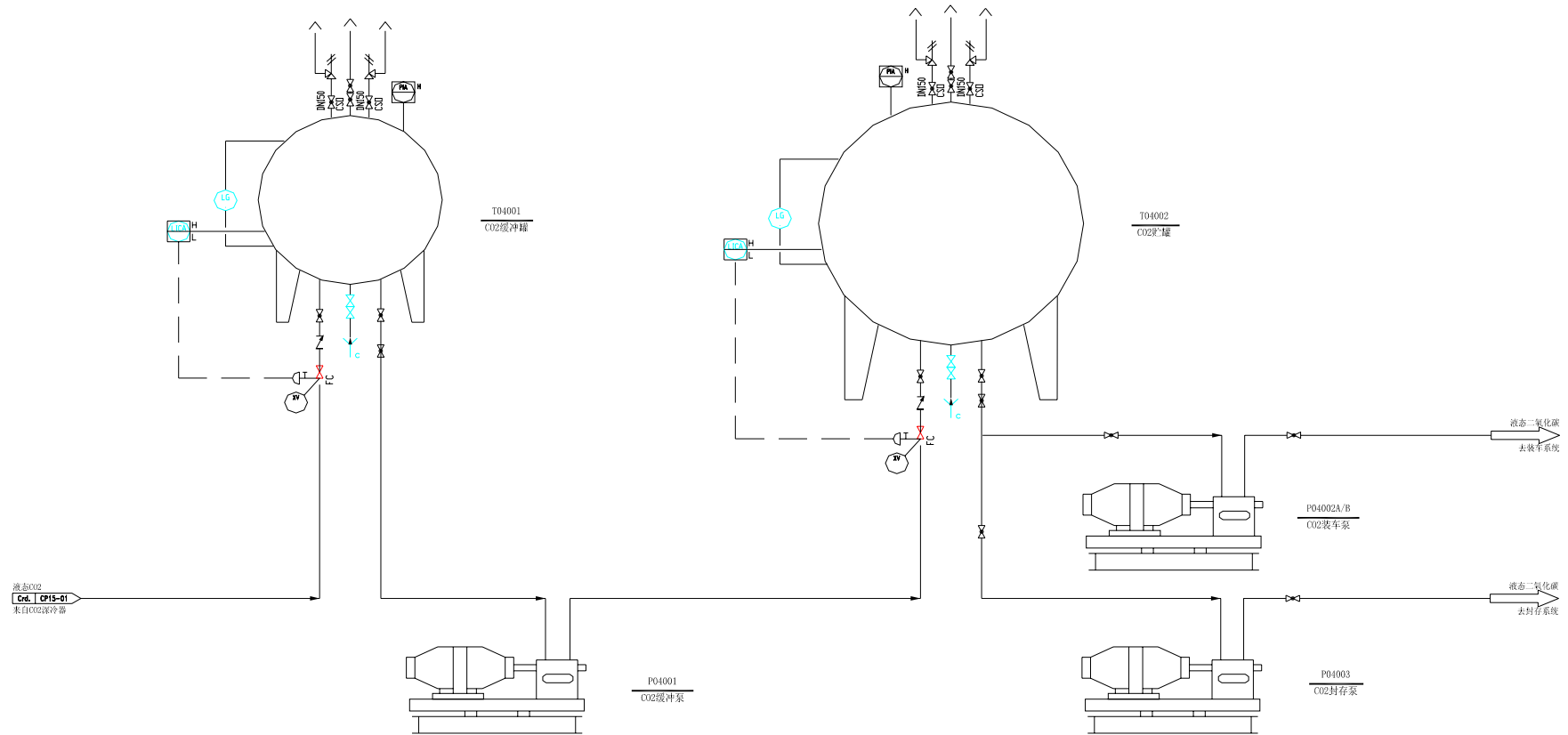
# \_Process Flow Diagram (compression, purification, liquefaction and rectification)



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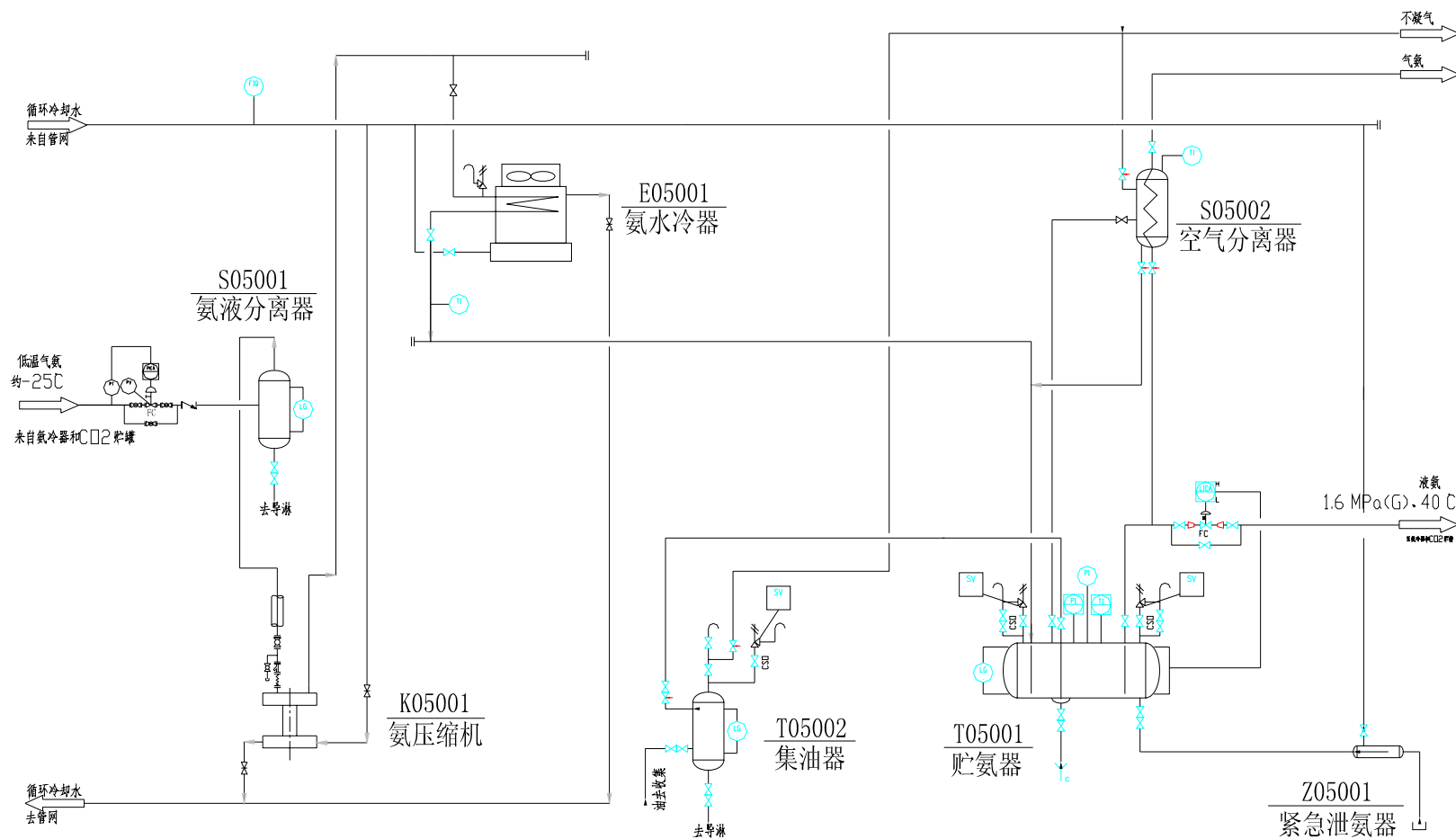
# \_Process Flow Diagram (Including transportation and intermediate storage)



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# \_Process Flow Diagram (refrigeration system)



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## \_Utilities Consumption

Electricity	220V、 50HZ	kW	100
	380/6k/10kV、 50HZ	kW	2108
Cooling water	P=0.4~0.5MPa $\Delta t=12^{\circ}\text{C}$	t/h	254
Steam	$T \geq 180^{\circ}\text{C}$	t/h	0.5



## 4. Capital Investment Estimate

- Total investment of the project: ~2 00 MRMB

including:

Construction investment ~190 MRMB



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## \_Cost Analysis

CCS cost	RMB/t CO <sub>2</sub>	277.12	41\$/t
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- CCS cost is 41\$/t which is lower than 100-120 \$/t as estimated for regular CCS projects abroad, which indicates:
  - CO<sub>2</sub> rich feed from CO<sub>2</sub> removal/capture process integrated in a chemical project like CTL benefits the decrease of CCS cost and favors CCS deployment.

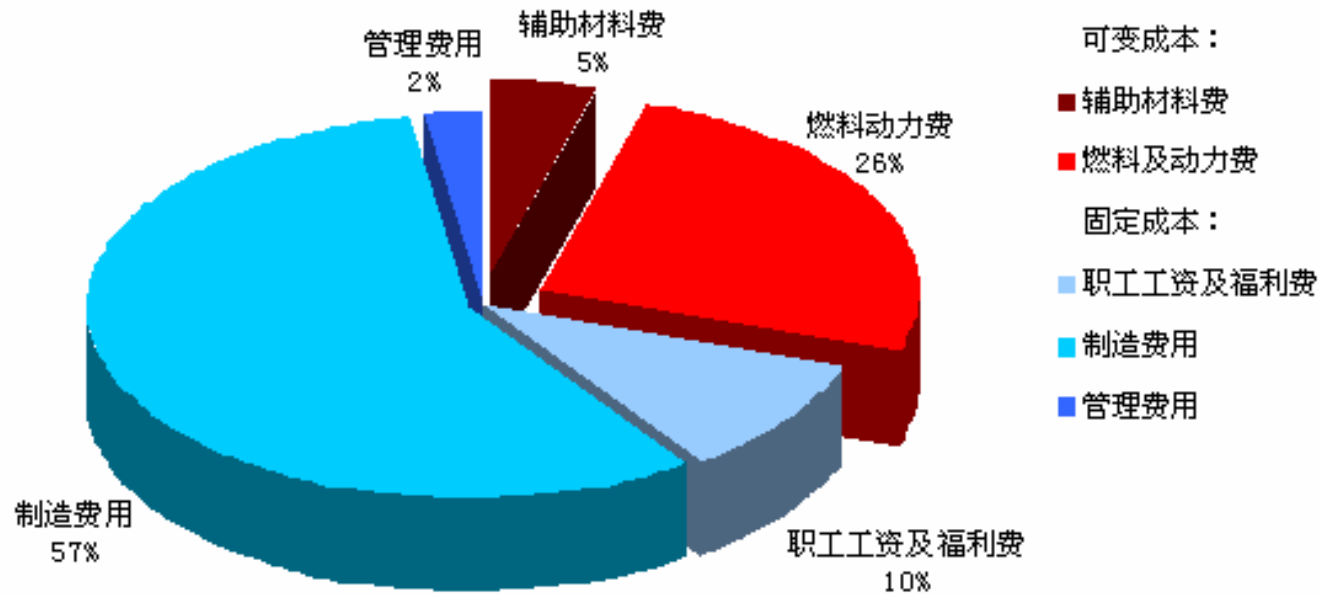


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方案一单位成本分析图 1



The variable cost : 31%, the fixed cost totally is 69%.  
The fixed cost goes down as the capacity rises up.  
The cost for a commercial project with over million tons/a injection will be lower than 41\$/t.





方案一单位成本分析图 2



The cost of capture and transportation accounts for 56%, lower than the portion(70-80% )of regular CCS project, while the cost of injection accounts for 44%, higher than the portion(20-30%) of regular CCS project as estimated. As the storage reservoir investment has a little relation to the capacity, the cost for million tons /a project will be lower than 41\$/t.



## 5 Study Conclusion

- ✓ Selected capture process for CO<sub>2</sub> rich source is mature and reliable with low operation cost and investment.
- ✓ The cost analysis indicates that CO<sub>2</sub> source which is the tail gas from CO<sub>2</sub> removal of a chemical complex benefits the decrease of CCS cost.
- ✓ Commercial CCS project is best to focus on CO<sub>2</sub> rich sources.



*THANKS  
FOR YOUR ATTENTION!*

Q&A

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