

Numerical Simulation of Water Rock Interaction and Fluid Flow

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CAGS WORKSHOP II'2010



China Australia Geological Storage of CO₂
中澳二氧化碳地质封存



Outline

1. Introduction
2. Geochemical Modelling
3. Full Physics Compositional Simulation
4. Case Study
5. Summary



1 Introduction

Trapping Mechanisms for CO₂ Storage Process in Saline Aquifer

- Hydrodynamic and structural trapping
- Solubility trapping
 - Storing CO₂ as a soluble component in brine
- Residual gas trapping
 - Trapping as immobile residual gas (Sgrm)
- Mineralization trapping
 - Water-rock interaction
 - Long-term storage of green house gas

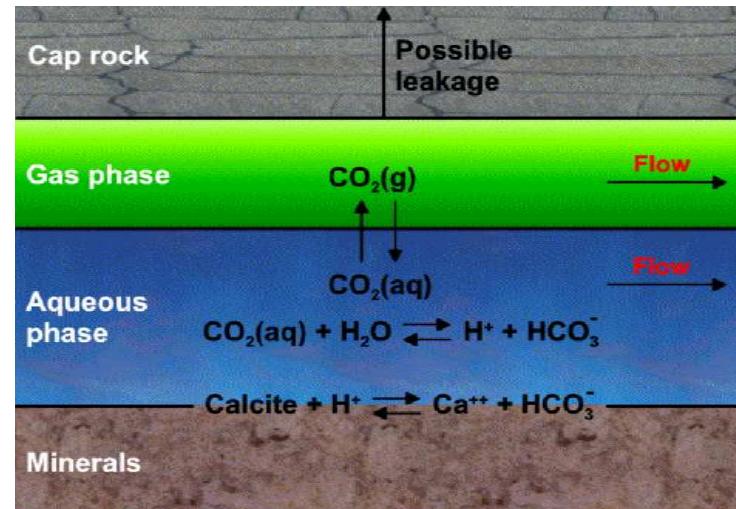


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Full-Physics Compositional Simulation

- Convective and dispersive flow
- Relative permeability hysteresis
- Gas solubility in aqueous phase
- Aqueous chemical equilibrium reactions
- Mineral dissolution and precipitation kinetics
- Vaporization of H₂O
- Predictions of brine density and viscosity
- Leakage through cap rock and thermal capability



CMG Training, 2008



What reactions could be critical?

- As injected CO₂ dissolves in formation water, it produces a weak acid (carbonic acid) which can chemically react with minerals in the host reservoir rock. Some of these reactions can result in the precipitation of new minerals and solid compounds in the formation pore space, effectively trapping the injected CO₂ (IPCC, 2005, Chevron Australia, 2005).
- In most geological strata, the formation of calcium, magnesium, and iron carbonates is expected to be the primary mineral trapping process (White et al. 2001, 2002, 2004, 2005).

2 Geochemical Modelling

- **Static equilibrium model**

- Solution of coupled non-linear equations

- **Closed system kinetic model**

- Solution of coupled non-linear ordinary differential equations

- **Flowing system**

- Solution of coupled non-linear partial differential equations

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Static Equilibrium Model

➤ Input:

- ✓ Water Analysis
- ✓ Thermodynamic Database
- ✓ Temperature
- ✓ Pressure

➤ Output:

- ✓ Saturation Index and Aqueous Speciation
- ✓ Charge Balance
- ✓ Modification to Downhole Conditions
- ✓ Geothermometers

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Fundamental Concepts (1)

➤ Charge Balance:

$$\frac{\sum (\text{molality} \times \text{charge})_{\text{Cations}} - \sum (\text{molality} \times \text{charge})_{\text{Anions}}}{\sum (\text{molality} \times \text{charge})_{\text{Cations}} + \sum (\text{molality} \times \text{charge})_{\text{Anions}}} \times 100$$

--More than +/-5% indicates problems with major components in aqueous phase.

➤ CO₂ Pressure in equilibrium with the fluid:



--Atmospheric log PCO₂=-3.5

If fluid PCO₂ > atmospheric, degassing occurs

If fluid PCO₂ < atmospheric, adsorption from atmosphere occurs



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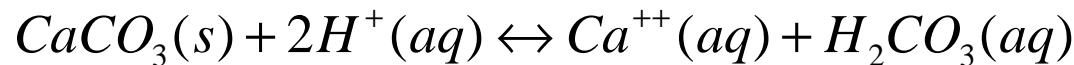
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Fundamental Concepts (2)

➤ Law of Mass Action:

Any reaction at EQUILIBRIUM, the activity product is a constant (**K_{eq}**) at a given temperature and pressure. For example,



$$Q = \frac{a_{Ca^{++}(aq)} \cdot a_{H_2CO_3(aq)}}{a_{CaCO_3(s)} \cdot a_{H^+}}^2$$

➤ Activity = Concentration × Activity Coefficient

The activity of a pure solid (e.g. **CaCO₃(s)**) is generally 1.0



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Chemical Equilibrium Between Aqueous Species

- Fast reversible aqueous reactions are modeled with chemical equilibrium reactions
 - ✓ Instantaneous and no rate associated with them.
- Typical reaction:



- The concentrations of the species in solution are determined from chemical equilibrium constants

$$K_{eq}(T) = \frac{a_{H^+} \cdot a_{HCO_3^-}}{a_{CO_2(aq)} \cdot a_{H_2O}}$$

‘ a ’ is the activity which is also a measure of concentration.



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Aqueous Species

➤ Activities of aqueous species:

$$a_{H_2O} \approx 1$$

$$a_i = \gamma_i \cdot m_i$$

γ_i = activity coefficient of species i

m_i = molality of species i (moles i / kgH₂O)

➤ Activity coefficient models

- ❖ Ideal solution: $\gamma_i = 1$
- ❖ Debye-Hückel model
- ❖ B-dot model



B-dot Model

$$\log \gamma_i = -\frac{Az_i^2 \sqrt{I}}{1 + \dot{a}_i B \sqrt{I}} + \dot{B}I$$

$$I = \frac{1}{2} \sum_{k=1}^{n_{aq}} m_k z_k^2$$

I = ionic strength

m_k = molality of component k

z_k = charge of component k

\dot{a}_i = ion size parameter of component i

A, B, \dot{B} = temperature - dependent parameters



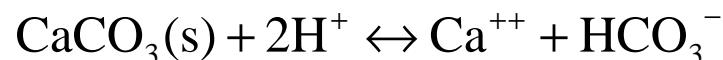
pH Value

► Definition: $-\log_{10}(a_{\text{H}^+})$

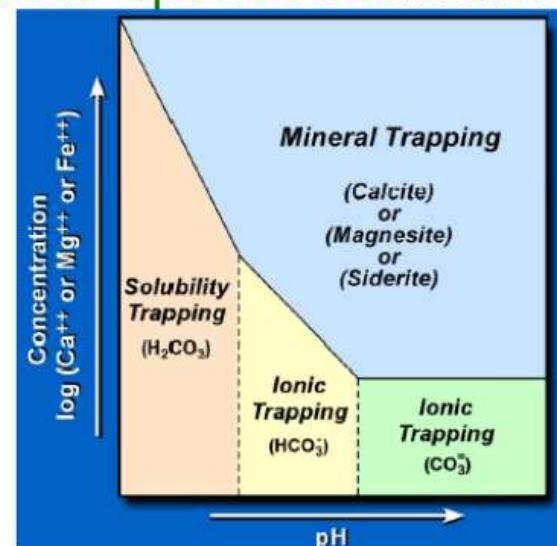
a_{H^+} is the activity of the hydrogen ion in the solution.

The pH is of critical importance in determining the behaviour of many ions and solids in solutions.

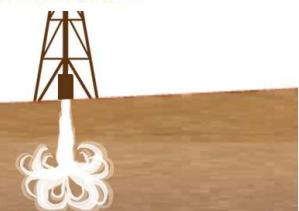
e.g.,



Aqueous Species Dominance Diagram



After Gunter
et al., 2004



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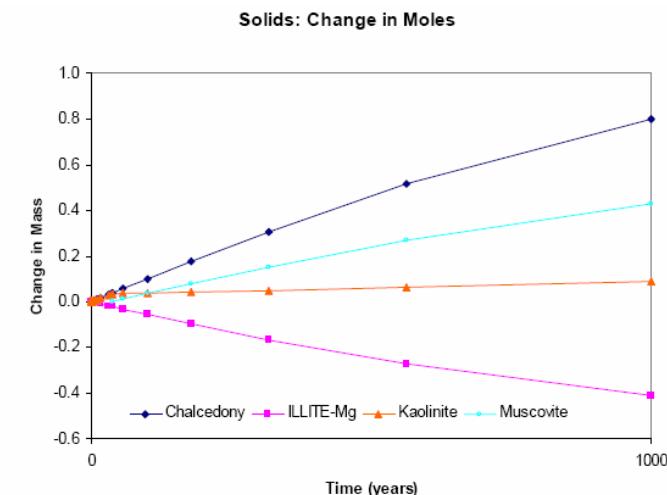
Closed System Kinetic Model

➤ Input:

- ✓ Static equilibrium modelling results
- ✓ Mineral Characteristics
- ✓ Kinetic Database
- ✓ Time

➤ Output:

- ✓ Saturation Index with Time
- ✓ Mineral Mass Changes
- ✓ Gas Uptake
- ✓ Solution Composition with Time

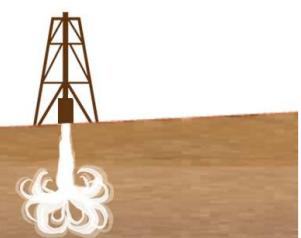


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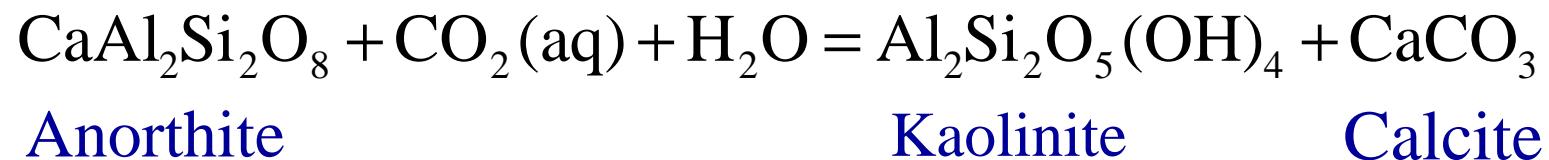
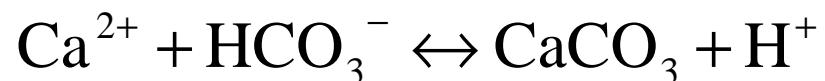


Unstable Minerals under Acidic Environment (Examples)

- Geochemical modelling considers all kinds of chemical reactions
- Carbonate mineral:
 - Calcium, magnesium, and iron carbonates
- Feldspar:
 - Potassium-feldspar to Anorthite, etc.
- Clay minerals:
 - Kaolinite, Illite, Smectite, etc.
- Volcanic clastics (?)
- Others (?)



Simple Example of Water-Rock Interaction



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Reaction Rate

Reaction Rates

Phases	Fast	Intermediate	Slow
carbonate	★		
salts	★		
feldspar			★
quartz			★
oxides/hydroxides	★	★	★
sulfides		★	
clays		★	★
homogeneous (water, gas & oil)	★	★	

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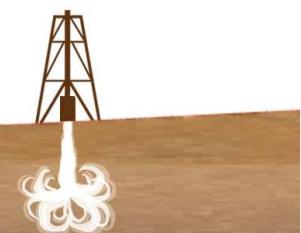
$$k = k_0 \exp \left[-\frac{E_a}{R} \left(\frac{1}{T} - \frac{1}{T_0} \right) \right]$$

k : reaction rate at temperature T

k_0 : reaction rate at temperature T_0

E_a : activation energy

R : gas constant



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3 Full Physics Compositional Simulation

➤ Input:

- ✓ Important chemical reactions based on the kinetic modelling
- ✓ Reservoir Characteristics (eg. Relperm, porosity, saturation, etc.)
- ✓ PVT
- ✓ Injection/Production History

➤ Output:

- ✓ Fluid Composition
- ✓ Mineralogical Changes
- ✓ Flow Paths
- ✓ Phase Redistribution



Mineral Dissolution & Precipitation



$$\frac{V}{\Delta t} (N_i^{n+1} - N_i^n) = r_i$$

$$r_i = V \cdot A \cdot k \cdot \left(1 - \frac{Q}{K_{eq}}\right)$$

$$Q = \frac{a_{\text{Ca}^{++}} \cdot a_{\text{HCO}_3^-}}{a_{\text{H}^+}}$$

V = bulk volume (m^3)

A = reactive surface area (m^2/m^3)

k = rate constant ($\text{mol}/\text{m}^2 \text{ s}$)

K_{eq} = chemical equilibrium constant

Q/K_{eq} = saturation index

$Q/K_{eq} > 1 \rightarrow$ mineral precipitation

$Q/K_{eq} < 1 \rightarrow$ mineral dissolution

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Material Balance Equation for CO₂

$$\begin{aligned} & \Delta T_g y_{CO_2,g} \Delta \Phi_g + \\ & \Delta T_w (y_{CO_2,aq} + y_{HCO_3^-,aq} + y_{CO_3^{--},aq}) \Delta \Phi_w \\ & + r_x + q_{CO_2(g)} + q_{CO_2(aq)} + q_{HCO_3^-} + q_{CO_3^{--}} \\ & - \frac{V}{\Delta t} [(N_{CO_2} + N_{HCO_3^-} + N_{CO_3^{--}})^{n+1} - \\ & (N_{CO_2} + N_{HCO_3^-} + N_{CO_3^{--}})^n] = 0 \\ N_{CO_2} &= N_{CO_2(g)} + N_{CO_2(aq)} \end{aligned}$$

T_{ij} - molar transmissibility of component i in phase j

y_{ij} - molar fraction of component i in phase j

V - gridblock bulk volume (m³)

q_i - molar injection rate of component i (mol/day)

N_i - moles of component i per gridblock volume

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Geochemical Reaction Selection in the Numerical Simulator

Reaction Selection | Mineral Reaction Data | Aqueous Phase Property Models | Aqueous Phase Gas Solubility |

Reaction Type Selection

- Aqueous Species Reactions
- Mineral Species Reactions

Chemical Equilibrium Equation Derivatives

- Analytical
- Numerical

Additional Component Selection

- Include Na⁺ and Cl⁻ ions

Mineral Precipitation/Dissolution Rate Equation Derivatives

- Analytical
- Numerical

Available Reactions

```

NpO2HPO4 = (HPO4-) + (NpO2++)
(NpO2HP04) = (HPO4-) + (NpO2+)
NpO2OH + (H+) = H2O + (NpO2+)
(NpO2OH+) + (H+) = H2O + (NpO2++)
NpO2SO4 = (SO4-) + (NpO2++)
(NpO2S04) = (SO4-) + (NpO2+)
(NpOH++) + (H+) = H2O + (Np++)
(NpOH++) + (H+) = (Np++) + H2O
(NpSO4++) = (Np++) + (SO4-)
(OH-) + (H+) = H2O
(P2O7-) + H2O = 2 (HPO4-)
(PO4-) + (H+) = (HPO4-)
PbCO3 + (H+) = (Pb++) + (HCO3-)
(PbCl+) = (Pb++) + (Cl-)
PbCl2 = (Pb++) + 2 (Cl-)
(PbCl3) = (Pb++) + 3 (Cl-)
(PbCl4) = (Pb++) + 4 (Cl-)
(Pbf+) = (Pb++) + (F-)
PbF2 = (Pb++) + 2 (F-)
(PbH2PO4) = (Pb++) + (H+) + (HPO4-)
PbHPO4 = (Pb++) + (HPO4-)
(PbPO4) + (H+) = (Pb++) + (HPO4-)

```

Selected Reactions

CO₂(aq) + H₂O = (H⁺) + (HCO₃⁻)
(CO₃²⁻) + (H⁺) = (HCO₃⁻)

Reaction Selection | Mineral Reaction Data | Aqueous Phase Property Models | Aqueous Phase Gas Solubility |

Reaction Type Selection

- Aqueous Species Reactions
- Mineral Species Reactions

Chemical Equilibrium Equation Derivatives

- Analytical
- Numerical

Additional Component Selection

- Include Na⁺ and Cl⁻ ions

Mineral Precipitation/Dissolution Rate Equation Derivatives

- Analytical
- Numerical

Available Reactions

```

Jarosite-Na + 6 (H+) = 2 (SO4-) + 3 (Fe+++) + 6 H2O + (Na+)
K(UO2)(AsO4)(c) = (UO2++) + (AsO4-) + (K+)
K-feldspar + 4 (H+) = 2 H2O + (K+) + (Al++) + 3 SiO2(aq)
K2CO3^3/2H2O + (H+) = 2 (K+) + (HCO3-) + 1.5 H2O
K2Cr2O7 + H2O = 2 (K+) + 2 (H+) + 2 (CrO4-)
K2CrO4 = 2 (K+) + (CrO4-)
K2Se = 2 (K+) + (Se-)
K8H4(CO3)6^3H2O + 2 (H+) = 8 (K+) + 6 (HCO3-) + 3 H2O
KBr = (K+) + (Br-)
KMgCl3 = (K+) + (Mg++) + 3 (Cl-)
KMgCl3^2H2O = (K+) + (Mg++) + 2 H2O + 3 (Cl-)
KNaCO3^6H2O + (H+) = (K+) + (Na+) + (HCO3-) + 6 H2O
KTcO4(s) = (K+) + (TcO4-)
Kainite = (K+) + (Mg++) + (Cl-) + (SO4-) + 3 H2O
Kalcicrite = (K+) + (HCO3-)
Kalsilite + 4 (H+) = 2 H2O + (K+) + (Al++) + SiO2(aq)
Kasolite + 4 (H+) = (UO2++) + (Pb++) + SiO2(aq) + 3 H2O
Kieserite = (Mg++) + (SO4-) + H2O
Kyanite + 6 (H+) = 3 H2O + 2 (Al++) + SiO2(aq)
Larnite + 4 (H+) = 2 (Ca++) + SiO2(aq) + 2 H2O
Laumontite + 8 (H+) = 8 H2O + (Ca++) + 2 (Al++) + 4 SiO2(aq)
Lawrencite = (Fe++) + 2 (Cl-)

```

Selected Reactions

Anorthite + 8 (H+) = 4 H2O + (Ca++) + 2 (Al++) + 2 SiO2(aq)
Calcite + (H+) = (Ca++) + (HCO3-)
Kaolinite + 6 (H+) = 5 H2O + 2 (Al++) + 2 SiO2(aq)

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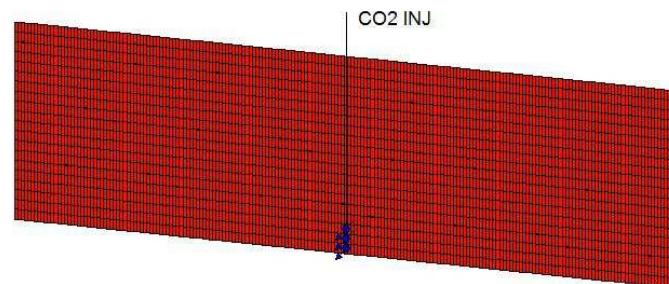
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4 Case Study: Case 1

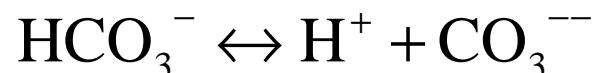
➤ CO₂ Injection at the Middle of Reservoir:

- Grid Dimension: 5m × 10m × 5m
- Grid Number: 200 × 1 × 20
- Dip angle of grid system: 2.0 degree
- Porosity: 0.18
- Permeability: 100md, Kv/Kh=1
- Sgrm = 0.2
- Injection Well: (101, 1, 1)
- Perforation Interval: (101, 1, 18) to (101, 1, 20)
- Injection Rate: 1×10^4 m³/day (STG surface gas rate)
- Injection Period: 2000-1-1 to 2003-1-1
- Simulation Period: 2000-1-1 to 2200-1-1
- Volume Fraction: Anorthite (1%), Calcite (1%) & Kaolinite (2%)

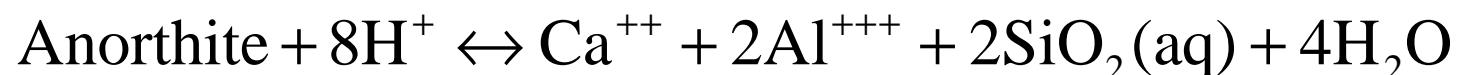
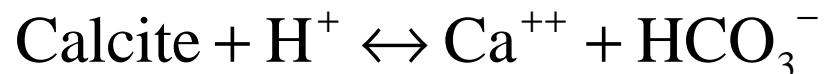


Aqueous & Mineral Reactions

Aqueous species reaction:



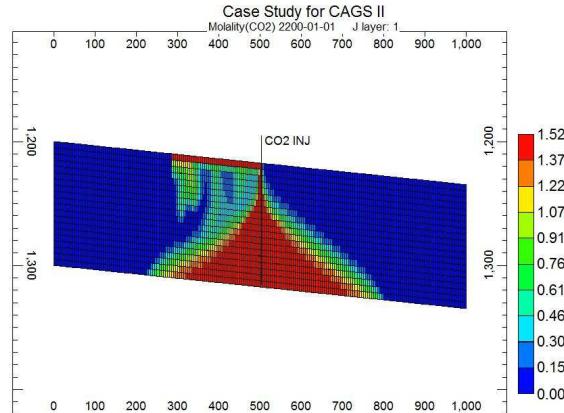
Mineral species reaction:



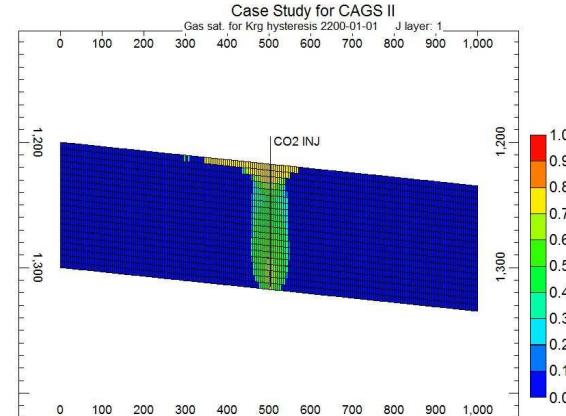
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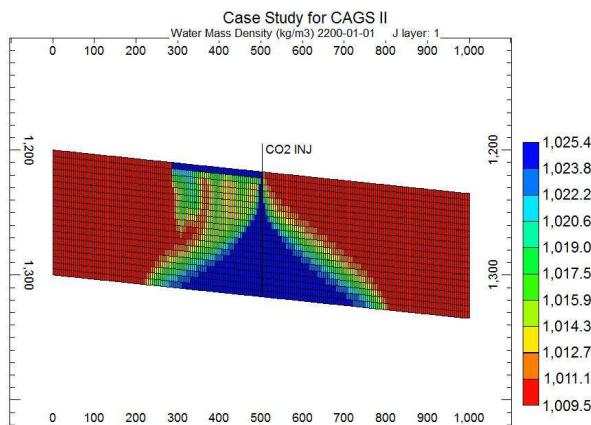
Simulation Results (200yrs) (1)



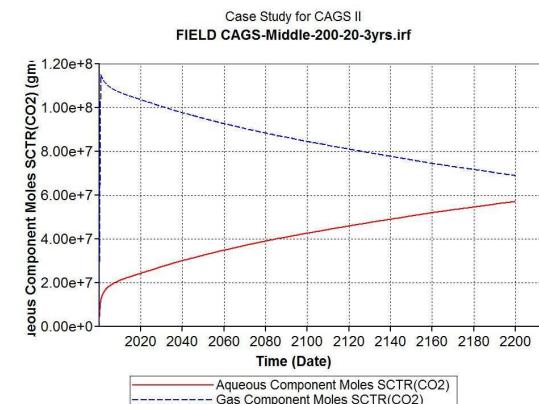
CO₂ Molality



Gas sat. for Krg hysteresis



Water Mass Density



Moles of Aqueous and Gas CO₂

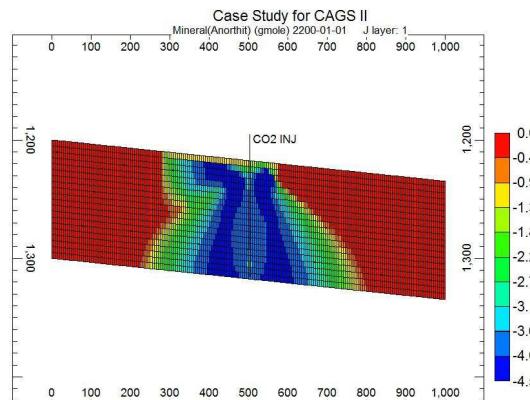
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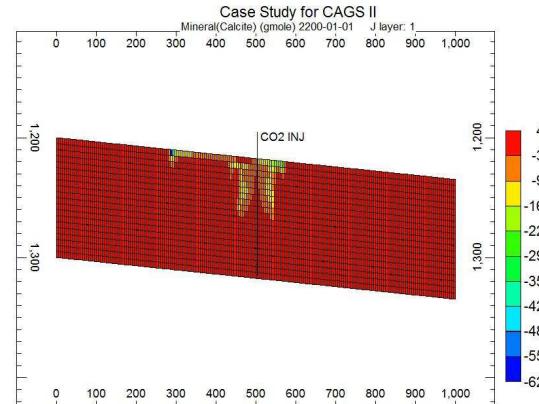
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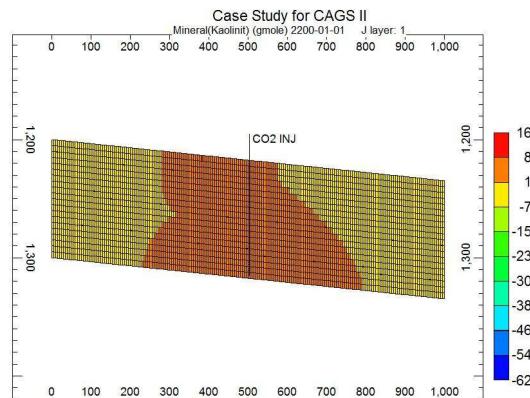
Simulation Results (200yrs) (2)



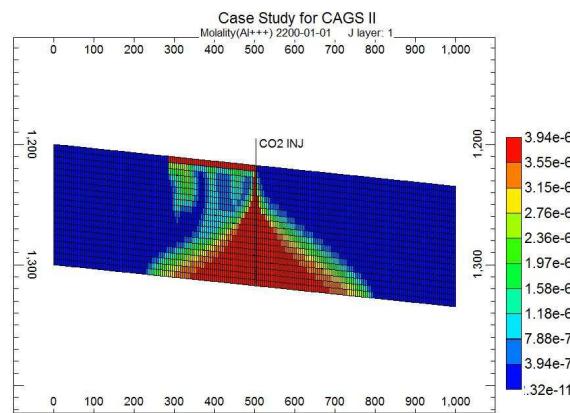
Molality of Anorthite



Molality of Calcite



Molality of Kaolinite



Molality of Al⁺⁺⁺

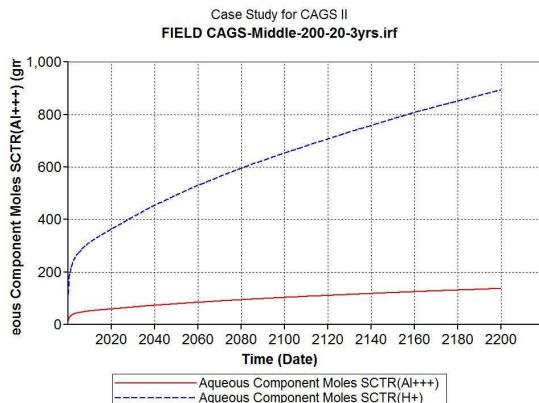
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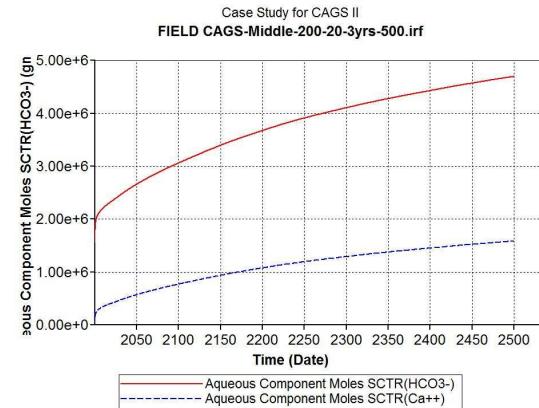
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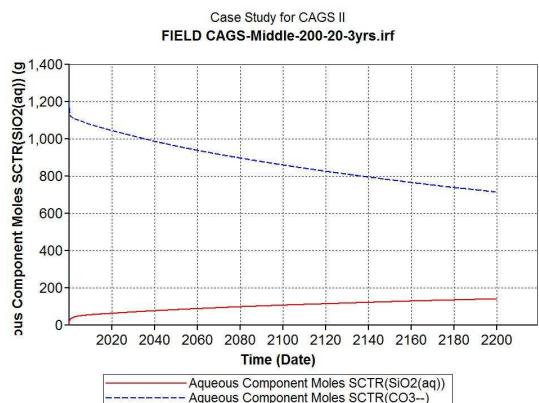
Simulation Results (200yrs) (3)



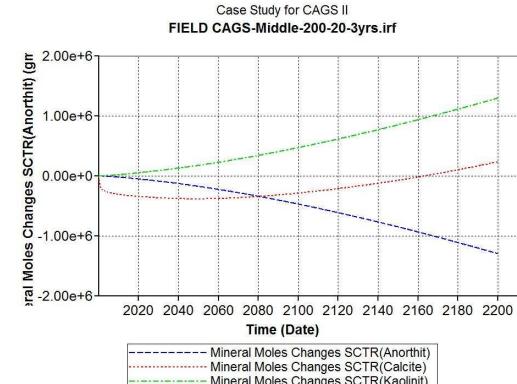
Moles of Al⁺⁺⁺ & H⁺



Moles of Ca⁺⁺ & HCO₃⁻



Moles of SiO₂ & CO₃⁻²



Moles of Minerals

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Simulation Results of Case I (200yrs)

➤ Total Cum Inj, mol = 1.28126E+08

➤ 3 years later:

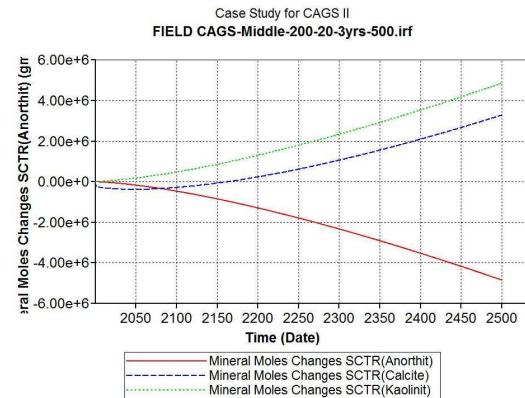
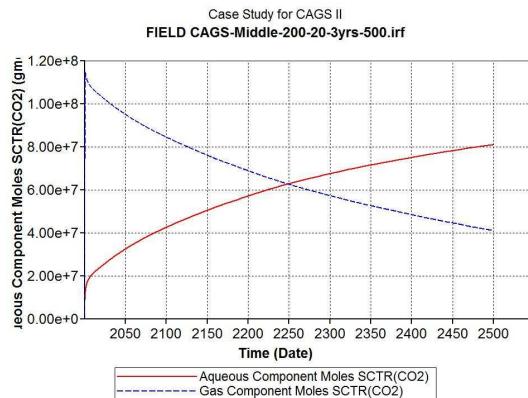
CO ₂ Storage Amounts in Reservoir	Moles	kg
Supercritical Phase	= 1.11307E+08	4.89863E+06
Trapped due to Hysteresis	= 2.42978E+07	1.06934E+06
Dissolved in Water	= 1.68263E+07	7.40524E+05
Present in Aqueous Ions	= 2.06357E+06	9.08176E+04
Present in Mineral Precipitate	= -2.50461E+05	-1.10228E+04

➤ 200years later:

CO ₂ Storage Amounts in Reservoir	Moles	kg
Supercritical Phase	= 6.89380E+07	3.03396E+06
Trapped due to Hysteresis	= 4.11539E+07	1.81118E+06
Dissolved in Water	= 5.71292E+07	2.51426E+06
Present in Aqueous Ions	= 3.67423E+06	1.61703E+05
Present in Mineral Precipitate	= 2.35526E+05	1.03655E+04



Long-Term Storage



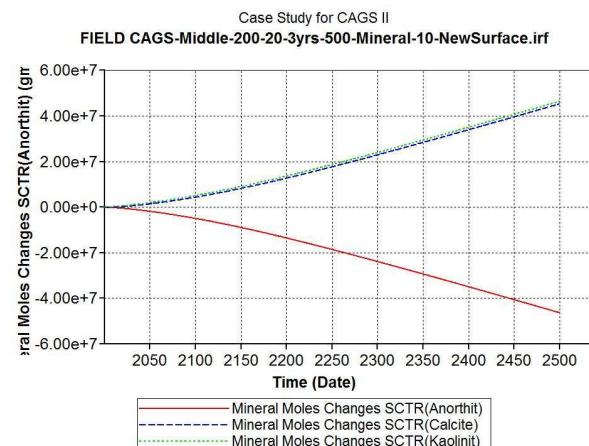
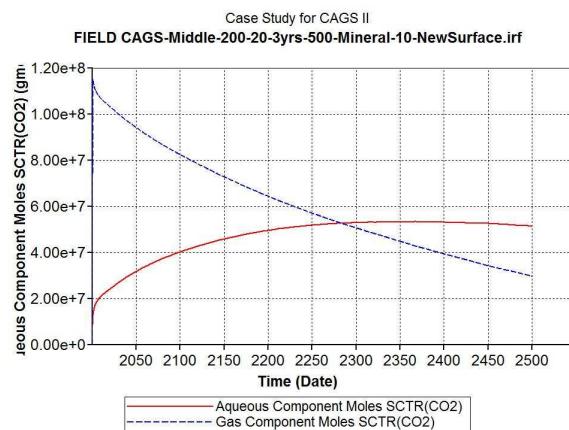
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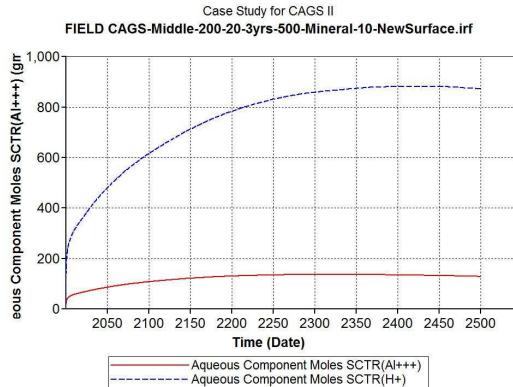


Influence of Mineral Content (Case 2)

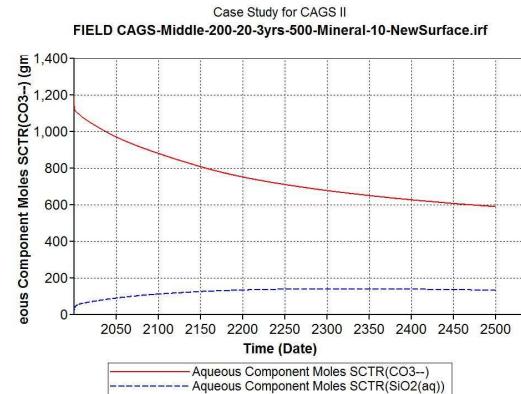
- Volume Fraction: Anorthite (10%), Calcite (10%) & Kaolinite (2%)
- Other conditions same as in Case 1



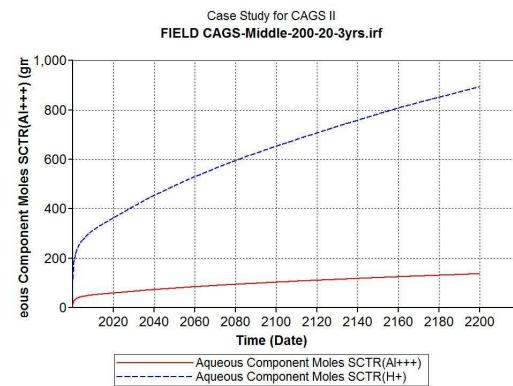
Influence of Mineral Content



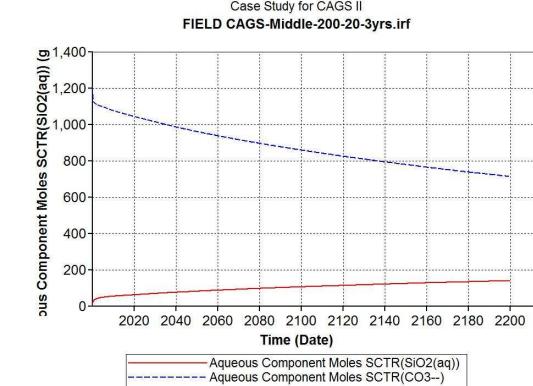
Moles of Al⁺⁺⁺ & H+ (Case 2)



Moles of CO₃⁻⁻ & SiO₂ (Case 2)



Moles of Al⁺⁺⁺ & H+ (Case 1)



Moles of CO₃⁻⁻ & SiO₂ (Case 1)

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5 Summary

- Analyses on the chemical properties of aqueous phase and initial mineral components are critical before numerical simulation process.
- Geochemical modelling (static equilibrium model and closed system kinetic model) provides understandings of geochemical evolution after CO₂ injection through modelling saturation index, solution composition and mineral mass with time. Hence the important chemical reactions will be advised for the full-physics compositional simulator.
- Based on the combinations of fluid flow dynamics and the selection of important geochemical reactions, the coupled simulation is able to provide information on CO₂ plume movement, effective storage capacity together with changes of minerals of rock, chemical properties (ions) of brine water and petrophysical properties.
- Mineral precipitation will be significant for safe long-term storage of CO₂ in saline aquifer.



China Australia Geological Storage of CO₂

中澳二氧化碳地质封存



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Liuqi Wang & Rick Causebrook
Geoscience Australia

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